Reactions of Butane and Isobutane Catalysed by Titanium Oxide treated with Sulphate Ion. Solid Superacid Catalyst¹

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Summary Solid superacid catalyst was obtained by exposing $H_4 TiO_4$ to $1 \times H_2 SO_4$ and then calcining in air at 500 °C; this catalyst was active for skeletal isomerizations of butane and isobutane.

SOLID superacid has many advantages as a catalyst compared with liquid superacid. We have synthesized a solid superacid which can be used at temperatures up to 500 °C. The catalyst can be prepared with ease by treating H_4TiO_4 with sulphate ion followed by calcination, and is catalytically active for reactions of butane and isobutane which are generally catalysed by superacids such as SbF_5-HF^2 or $SbF_5-SiO_2-Al_2O_3$.³

A typical preparation of the catalysts was as follows. H_4TiO_4 -I was obtained by dissolving titanium(rv) isopropoxide in aqueous nitric acid, hydrolysing with aqueous ammonia, washing the precipitate, and drying at 100 °C. H_4TiO_4 -II was prepared by hydrolysing aqueous TiCl₄ with aqueous ammonia followed by washing and drying. The catalyst was treated with sulphate ion by pouring 1 N H_2SO_4 (30 ml) on to the dried titanium material (2 g) on a filter paper. The materials were dried and powdered below 100 mesh, calcined in a Pyrex tube in air at 500 °C for 3 h, and finally sealed in an ampoule until use. The catalysts thus prepared from H_4TiO_4 -I and -II were referred to as TiO₂-I and -II, respectively. Each catalyst was again

heated in air at 450 °C for 1.5 h before reaction. Reactions were carried out in a recirculation reactor of *ca.* 170 ml using 1.0 g of the catalyst and 7.8 ml (N.T.P.) of the hydrocarbon. The reaction products were analysed by g.l.c. using a 1 m column of Porapak R.

Both $\text{TiO}_2\text{-I}$ and $\text{TiO}_2\text{-II}$ catalysts⁺, were active for the skeletal isomerization of butane at room temperature. Isobutane was produced in 4% yield after 24 h and in 8% yield after 48 h, together with trace amounts of propane. The results of the reactions of butane and isobutane at 50 °C are shown in the Table. Pentane, isopentane, and hexane were observed as products in addition to propane and the isomers of the reactants. For butane, the catalytic activity of TiO₂-I was higher than that of TiO₂-II, although the latter catalyst had a higher selectivity for skeletal isomerization, when isobutane was obtained in 93% yield after 48 h. The catalytic activity of TiO₂-I was lower for isobutane than for butane.

Since these catalysts were calcined at 500 °C and hence can be used for reactions up to 500 °C reactions were carried out at high temperatures under pulse reaction conditions (flow rate of He carrier gas, 3 ml min⁻¹; catalyst amount, 0.35 g; pulse size, 0.02 ml). Butane was converted into isobutane in 5% yield at 170 °C, in 13% yield at 200 °C, and to isobutane and propane in 25, and 5% yields, respectively, at 230 °C in the first pulse over TiO_a-I .

[‡] The sulphate-treated catalyst showed i.r. absorption bands at 980, 1040, 1140, and 1240 cm⁻¹, which are assigned to the bidentate sulphate ion co-ordinated to the metal (see ref. 1).

Reactant	Time/h	Product distribution/%							
		Propane	Butane	Isobutane	Pentane	Isopentane	Hexane		
Butane	6	1.0	95.8	3.1	0	0	0		
	20	1.9	66.8	30.4	Trace	0.9	0		
	48	5.8	31.3	59.4	Trace	3.5	Trace		
	24ª	Trace	90·4	9.6	0	0	0		
	48ª	0.7	77.0	21.5	Trace	0.8	0		
Isobutane	24	Trace	3.0	97.0	Trace	Trace	0		
	48	0.7	5.6	91.9	Trace	1.8	0		
	96	1.2	8.5	85.1	0.7	4.5	Trace		

Table.	Reaction	of	butane a	nd	isobutane	over	TiO ₂ -I	at 50	°C.
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^a Reaction over TiO₂-II.

This catalyst also converted isobutane into butane in 4%yield at 140 °C and to butane and propane in 28 and 5% yields, respectively, at 170 °C in the first pulse.

SiO₂-Al₂O₃ (Shokubai Kasei Kogyo Ltd., 13% Al₂O₃, heat-treated at 500 °C), whose acid strength is in the range $-12\cdot70 <\!\!H_0 \leqslant -11\cdot35,^1$ was inactive for the reaction of butane at 50 °C and gave just $1\cdot5\%$ isobutane at 100 °C after 24 h. The acid strength of the present catalysts was examined by a colour change method using Hammett indicators,⁴ when indicator is added to a powdered sample

dissolved in solvent. TiO2-I and -II in dried sulphuryl chloride changed the basic form (colourless) of 2,4-dinitrotoluene (p $K_{\mathbf{a}} = -13.75$) to the conjugate acid form (yellow), and also changed the colour of 2,4-dinitrofluorobenzene (-14.52) slightly. Thus, the acid strength of the present superacid catalysts is estimated to be $-14.52 \ge H_0$.

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¹ For previous article in the series 'Solid catalysts treated with anions' see M. Hino and K. Arata, Chem. Letters, 1979, 1259.

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